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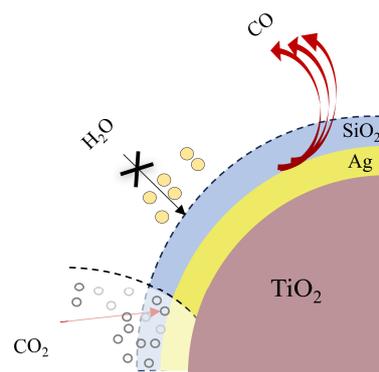
Porous SiO₂ Encapsulation for Selective Suppression of Hydrogen Evolution in Photocatalytic CO₂ Reduction

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Received: 3 December 2025; Revised: 2 February 2026; Accepted: 9 February 2026; Published: 25 February 2026

Abstract: Photocatalytic carbon dioxide reduction reaction (CO₂RR) represents a promising route for sustainable energy conversion. However, in conventional solid-liquid-gas reaction systems, inefficient CO₂ diffusion to the catalyst surface often leads to dominant hydrogen evolution reaction (HER), limiting CO₂ conversion efficiency and product selectivity. Herein, we propose a catalyst encapsulation strategy using porous silicon dioxide (SiO₂) to spatially control molecular transport toward the active sites. By encapsulating Ag-modified titanium dioxide within a porous SiO₂ layer, we effectively restrict water access to the catalytic interface while facilitating CO₂ permeation. As a result, the parasitic HER is significantly suppressed, enabling an exceptional 100% selectivity for CO production from photocatalytic CO₂ reduction in pure water, which is a dramatic improvement from the mere 5.9% CO selectivity of the unencapsulated Ag-TiO₂ catalyst. This design achieves near-complete suppression of HER and 100% selectivity toward CO production under photocatalytic conditions. Our work provides a versatile interfacial engineering approach to overcome mass transfer limitations in three-phase photocatalytic systems, opening avenues for efficient gas-involving photoreactions.

**Keywords:** CO₂RR; SiO₂ shell; core-shell; HER suppression; interface engineering

1. Introduction

With the rapid development of industry and economy globally, the massive consumption of finite fossil fuels has led to severe environmental issues, notably the greenhouse effect driven by rising atmospheric CO₂ levels [1–4]. In this context, photocatalytic CO₂ reduction reaction (CO₂RR) stands out as a promising strategy for converting solar energy into sustainable fuels, often regarded as the “holy grail” of energy conversion [5–8]. From the perspectives of sustainability and environmental friendliness, using water as the hydrogen source for CO₂RR is highly desirable [9,10]. However, a significant challenge persists in aqueous-phase photocatalytic CO₂RR, which is the severe competition from the hydrogen evolution reaction (HER) [11,12]. In typical aqueous reaction systems, HER tends to dominate over CO₂RR, primarily due to the kinetically more favorable proton reduction pathway. This fierce competition results in unsatisfactory selectivity for carbon-based products and low CO₂RR efficiency in most cases [13,14].

Although substantial efforts have been devoted to enhancing CO₂RR performance through catalyst design, such as developing novel semiconductors, morphology control, doping, and constructing heterojunctions [5,15–19], these strategies often focus on modifying the intrinsic electronic structure of the catalysts. For instance, Sun et al. designed an N, S-codoped Fe-based MIL-88B catalyst with a well-defined bipyramidal hexagonal prism morphology, achieving a high C₂H₄ yield of 17.7 μmol g⁻¹ h⁻¹ [20]. Meanwhile, Wang et al. anchored Ag single atoms on hollow porous polygonal C₃N₄ nanotubes to form a photocatalyst, showing up to 94% CO selectivity [21]. Despite these advances, effectively suppressing the competing HER to achieve near-unity product selectivity remains a critical and unresolved issue.



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Recent studies have highlighted that the interfacial microenvironment of the catalyst plays a decisive role in governing the reaction pathway [22]. The simultaneous presence of water molecules and CO₂ reactants at the catalyst surface creates a direct competition between HER and CO₂RR [23]. Therefore, precisely controlling the transport of key molecules (H₂O and CO₂) to the active sites is crucial for steering the selectivity. Conventional approaches, such as employing organic hole scavengers, can alter the reaction microenvironment but introduce problems like high cost, toxicity, and compromised sustainability [24,25].

To address the fundamental challenge of HER dominance, we propose an interfacial engineering strategy centered on selectively inhibiting the access of water to the catalytic active sites. Herein, we demonstrate a porous silicon dioxide (SiO₂) encapsulation layer coated on Ag-loaded TiO₂ photocatalysts (Ag-TiO₂@SiO₂). This design does not aim to enhance CO₂ diffusion but rather to create a localized hydrophobic microenvironment that preferentially restricts the migration of water molecules to the reaction interface while allowing CO₂ permeation. As a result, the parasitic HER is significantly suppressed, enabling an exceptional 100% selectivity for CO production from photocatalytic CO₂ reduction in pure water, which is a dramatic improvement from the mere 5.9% CO selectivity of the unencapsulated Ag-TiO₂ catalyst. This work provides a distinct and effective solution to the selectivity challenge by managing the interfacial reactant supply, opening new avenues for optimizing various multiphase photocatalytic processes.

2. Experimental Section

2.1. Materials and Methods

All chemicals were of analytical grade and used without further. TiO₂ nanoparticles (P25, Degussa, Germany) were used as the photocatalyst. AgNO₃ (99.8%), acetone (99.9%), ethanol (95%), tetraethyl orthosilicate (TEOS) and ammonia aqueous solution (28%) were purchased from Sinopharm Chemical Reagent Co. (Shanghai, China). Hexadecyl trimethyl ammonium Bromide (CTAB) was purchased from Shanghai Aladdin Biochemical Technology Co. (Shanghai, China). Deionized water (H₂O, 18.25 MΩ·cm) supplied by an UP-Water Purification System was used in the whole experimental process.

2.1.1. Synthesis of Ag-TiO₂

Ag nanoparticles were loaded onto the surface of TiO₂ to form Ag-TiO₂ nanoparticles using a photo-loading method. Water, methanol, and AgNO₃ were used as solvent, holes sacrificial agent, and Ag source, respectively. For the preparation of Ag-TiO₂, 0.2 g TiO₂ was dispersed in an aqueous solution containing 40 mL H₂O and 10 mL ethanol under sonication. Then, 0.5 mL AgNO₃ aqueous solution (50 mM) was added with vigorous stirring and continuously bubbled using high purity Ar gas for 30 min. Subsequently, the mixture was moved to a sealed transparent container and irradiated under a 300 W xenon lamp (Beijing China Education Au-light Co., Ltd. CEL-HXF300-T3) for 60 min. The as-prepared Ag-TiO₂ nanoparticles were separated by centrifugation and washed three times with water, and dried at 60 °C overnight.

2.1.2. Synthesis of Ag-TiO₂@SiO₂

The Ag-TiO₂@SiO₂ particles were prepared according to Stöber method. In a typical procedure, 100 mg Ag-TiO₂ and 300 mg CTAB were dispersed in the mixture of ethanol (80 mL) and water (20 mL) and 1 mL of ammonia aqueous solution (28 wt%) under stirring for 30 min, then 200 μL of TEOS was added slowly with continuous stirring for 2 h. The particles were collected by centrifugation and washed with ethanol and water, respectively. The CTAB surfactant was removed by solvent extraction method using 120 mL of acetone solution and refluxed at 80 °C for 48 h. This extraction process was repeated three times. After centrifugating and washing with ethanol and water, the Ag-TiO₂@SiO₂-2 core-shell nanocarriers were obtained. By altering the amount of TEOS to 50 μL or 400 μL, Ag-TiO₂@SiO₂-1 and Ag-TiO₂@SiO₂-3 were obtained. Ag-TiO₂@SiO₂-2 is commonly abbreviated as Ag-TiO₂@SiO₂.

2.1.3. Synthesis of Ag-TiO₂@D-SiO₂

In a typical procedure, 100 mg Ag-TiO₂ were dispersed in the mixture of ethanol (80 mL) and water (20 mL) and 1 mL of ammonia aqueous solution (28 wt%) under stirring for 30 min, then 200 μL of TEOS was added slowly with continuous stirring for 2 h. The particles were collected by centrifugation and washed with ethanol and water, the Ag-TiO₂@D-SiO₂ core-shell nanocarriers were obtained.

2.1.4. Synthesis of SiO₂

In a typical procedure, 300 mg CTAB were dispersed in the mixture of ethanol (80 mL) and water (20 mL) and 1 mL of ammonia aqueous solution (28 wt%) under stirring for 30 min, then 200 μL of TEOS was added slowly with continuous stirring for 2 h. The particles were collected by centrifugation and washed with ethanol and water, respectively.

2.1.5. Synthesis of Ag-TiO₂-CTAB

In a typical procedure, 100 mg Ag-TiO₂ and 300 mg CTAB were dispersed in the mixture of ethanol (80 mL) and water (20 mL) and 1 mL of ammonia aqueous solution (28 wt%) under stirring for 2 h. The particles were collected by centrifugation and washed with ethanol and water, respectively.

2.1.6. Synthesis of Ag-TiO₂@SiO₂-NaOH

Ag-TiO₂@SiO₂-NaOH were prepared by etching Ag-TiO₂@SiO₂ in 10 mL of 2 M NaOH solution at 80 °C for 1 h.

2.2. Characterization

High-resolution TEM (HRTEM) images, high-angle annular dark-field scanning transmission microscopy (HAADF-STEM) images, and energy-dispersive X-ray spectroscopy (EDS) elemental mappings and line scans were performed on a JEM-F200 microscope equipped with a built-in EDS operated at 200 kV. The powder X-ray diffraction (PXRD) patterns were obtained on a Rigaku SmartLab, using Cu Kα (λ = 0.15406 nm) radiation. Textural properties of the catalysts were measured by N₂ physisorption at -196 °C on Micromeritics ASAP 2460 instrument. X-ray photoelectron spectroscopy (XPS) was conducted using a Thermo Fisher ESCALAB Xi+ spectrometer equipped with monochromatic Al Kα radiations. The Ag 3d, Ti 2p, O 1s and Si 2p peaks, as well as the valence bands, were corrected using the C 1s contamination peak (284.8 eV) as a reference. The content of Ag of the samples were determined by inductively coupled plasma mass spectrometry (ICP-MS), using a PerkinElmer NexION 350D (Waltham, MA, USA). Water-droplet contact angle tests were performed on the JY-82B contact angle goniometer. An Intrinsic DVS instrument from Surface Measurement Systems was used to perform the water vapor adsorption and desorption experiments over a humidity range of 0 ~ 95%. Each humidity step was made if less than a 0.002% weight change occurred over 10 min, with a maximum hold time of 240 min.

2.3. Photocatalytic CO₂RR Measurements

The photocatalytic CO₂ reduction measurements were carried out in a sealed reaction system. A 300 W Xe lamp (Beijing China Education Au-light Co., Ltd. CEL-HXF300-T3) was used as the light source providing a full spectrum illumination. In the photocatalytic process, 5 mg catalyst powder and 20 mL water were placed in a quartz reactor with a window area of 16 cm² and a volume of 130 mL. Before reaction, the reactor was purged with high purity CO₂ (99.999%) for 30 min. During the reaction, the reactor was placed on a magnetic stirrer, and the stirring speed was set at 800 rpm. The reaction temperature is controlled at 25 °C with a water circulator. Reaction was stopped after 4 h. The gas products were quantitatively analyzed by a gas chromatograph (SHIMANZU GC-2014) equipped with flame ionization detector (FID) and thermal conductivity detector (TCD).

The isotope-labeling experiments were carried out under the same experimental conditions, except that ¹²CO₂ was replaced with ¹³CO₂. The ¹³C-labeled products were analyzed using a gas chromatograph-mass spectrometer (GC-MS, Agilent 5977B GC/MSD). In cycling measurements, the catalyst was washed with ultrapure water to remove surface adsorbates before each reaction cycle. In this work the selectivity of catalyst for CO₂ reduction to acetate was calculated by following equation:

$$\text{Selectivity (\%)} = n(\text{CO})/[n(\text{H}_2) + n(\text{CO}) + n(\text{CH}_4) + n(\text{C}_2\text{H}_4)] \times 100\%$$

where, $n(\text{H}_2)$, $n(\text{CO})$, $n(\text{CH}_4)$ and $n(\text{C}_2\text{H}_4)$ are the mole amounts of produced H₂, CO, CH₄ and C₂H₄, respectively.

3. Results and Discussion

The core-shell structured Ag-TiO₂@SiO₂ photocatalyst was synthesized via a two-step procedure, as illustrated in Figure 1a. Initially, Ag nanoparticles were deposited on the surface of TiO₂ through a photo-deposition process to form Ag-TiO₂ nanoparticles (Figure S1) [26]. Subsequently, a porous SiO₂ shell was encapsulated onto the Ag-TiO₂ nanoparticles using the Stöber method [27]. This rational design aims to selectively control the transport of reactant molecules (H₂O and CO₂) to the active sites by creating a physical barrier, thereby

addressing the critical issue of HER competing with CO₂RR in the three-phase photocatalytic system. The X-ray diffraction (XRD) patterns (Figure 1b) of both Ag-TiO₂ and Ag-TiO₂@SiO₂ are identical to that of the pristine TiO₂, showing a mixed phase of anatase and rutile. The absence of distinct Ag diffraction peaks is attributed to its low loading and high dispersion [28]. Transmission electron microscopy (TEM) images (Figure 1c) confirmed the successful encapsulation of Ag-TiO₂ nanoparticles by a uniform SiO₂ shell, typically 5–15 nm thick. High-resolution TEM (HRTEM) analysis (Figures 1d and S2) reveals lattice fringes of 0.352 nm and 0.236 nm, corresponding to the (101) plane of anatase TiO₂ and (111) plane of metallic Ag, respectively. Energy-dispersive X-ray spectroscopy (EDS) mapping (Figure 1e) further verifies the core-shell structure, showing a homogeneous distribution of Ag, Ti, and O elements in the core, while the Si signal forms a distinct shell surrounding the core.

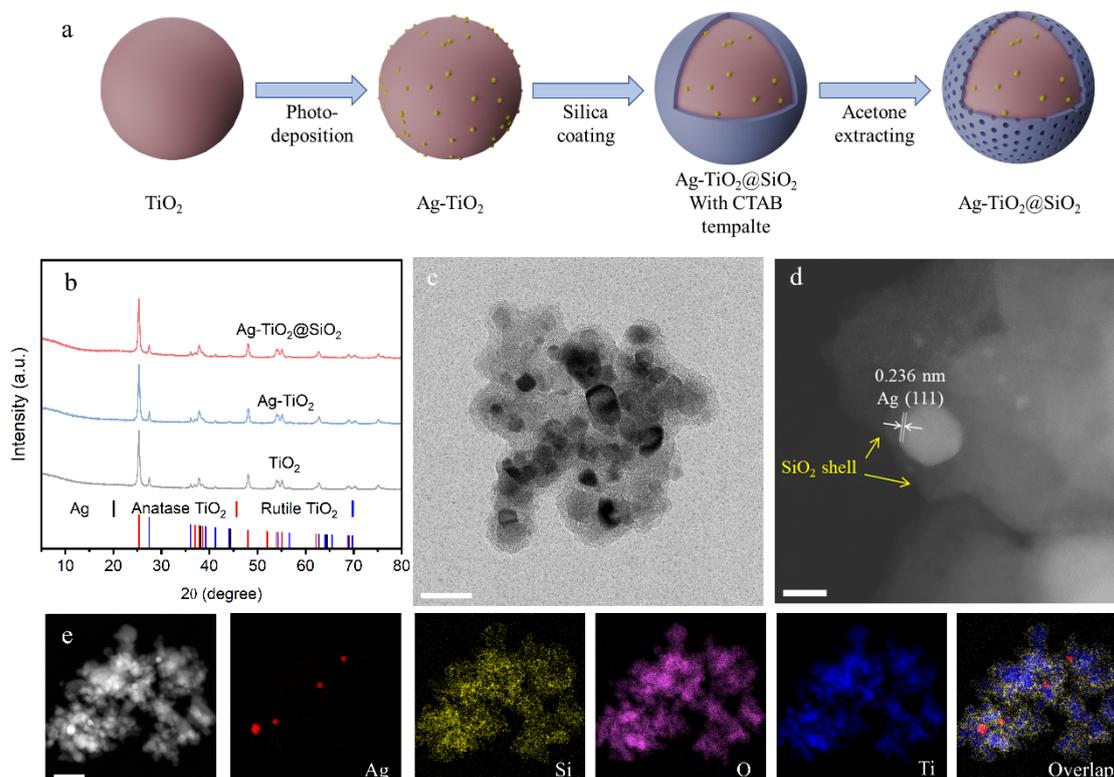


Figure 1. (a) Schematic illustration of the formation of Ag-TiO₂@SiO₂. (b) XRD patterns of TiO₂, Ag-TiO₂ and Ag-TiO₂@SiO₂. (c) TEM image of Ag-TiO₂@SiO₂, scale bars: 50 nm. (d) HRTEM image of Ag-TiO₂@SiO₂, scale bars: 5 nm. (e) STEM image of Ag-TiO₂@SiO₂ and corresponding element mapping (Ag, Si, O, and Ti), scale bars: 100 nm.

The chemical structures of the Ag-TiO₂ and Ag-TiO₂@SiO₂ nanoparticles were further examined by Fourier transform infrared (FTIR) spectroscopy. As shown in Figure 2a, the FTIR spectra offer clear evidence of functional groups and chemical bonds present in both samples. In each spectrum, the peak at 409 cm⁻¹ is associated with the Ti-O-Ti vibration of the TiO₂ crystal framework, confirming its presence as the primary component [29]. Additional peaks at 3445 cm⁻¹ and 1632 cm⁻¹ correspond to the O-H stretching and bending vibrations, respectively, indicating the presence of adsorbed water molecules on the nanoparticle surfaces. Notably, the Ag-TiO₂@SiO₂ sample exhibits a distinct peak at 1072 cm⁻¹, which is characteristic of the asymmetric stretching vibration of Si-O-Si bonds, confirming the successful formation of a SiO₂ shell. Also observable in the Ag-TiO₂@SiO₂ spectrum are several peaks associated with the structure-directing agent CTAB, including the C-N stretching vibration at 1481 cm⁻¹ and the -CH₂- rocking vibrations at 2922 cm⁻¹ and 2852 cm⁻¹ [27]. The presence of these organic residues suggests that CTAB is incorporated into the SiO₂ shell, which likely influences the material's final porosity and surface properties, which is crucial for forming the porous and hydrophobic shell.

X-ray photoelectron spectroscopy (XPS) was further conducted to probe the surface chemical states and elemental composition of Ag-TiO₂ and Ag-TiO₂@SiO₂ nanoparticles. As illustrated in Figure 2b, the XPS survey spectrum of Ag-TiO₂ exhibits distinct photoelectron peaks corresponding to Ag and Ti, indicating the presence of both metallic Ag and TiO₂ on the surface. In contrast, the survey spectrum of Ag-TiO₂@SiO₂ shows a substantial attenuation of the Ag and Ti signals, while new and prominent peaks corresponding to Si are observed (Figure S3). This marked decrease in signal intensity from the underlying Ag-TiO₂ core, coupled with the emergence of Si-related peaks, provides strong evidence

for the formation of a continuous and conformal SiO₂ shell layer coating the surface, which effectively shields the photoelectrons emitted from the core material, which is consistent with the TEM observations.

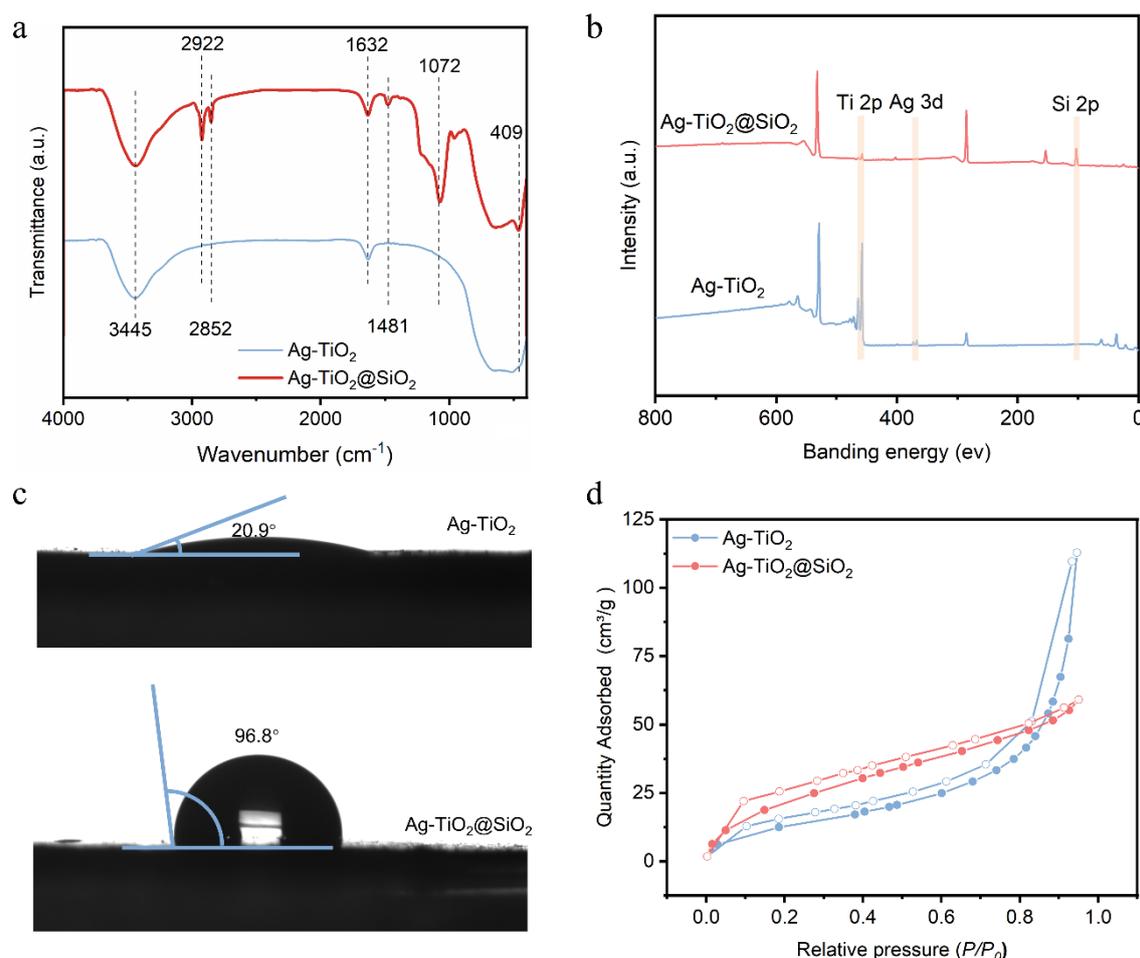


Figure 2. (a) FTIR spectra of Ag-TiO₂ and Ag-TiO₂@SiO₂, (b) XPS spectra of Ag-TiO₂ and Ag-TiO₂@SiO₂. (c) Water droplet contact angle tests. (d) The water vapor adsorption and desorption tests of Ag-TiO₂ and Ag-TiO₂@SiO₂.

To validate the role of the SiO₂ shell in modulating the interfacial microenvironment, we systematically characterized the surface physicochemical properties. Water contact angle measurements (Figure 2c) revealed that the pristine Ag-TiO₂ surface is hydrophilic (contact angle of 20.9°). In stark contrast, the Ag-TiO₂@SiO₂ surface exhibited a significantly increased contact angle of 96.8°, demonstrating that the SiO₂ coating effectively enhanced surface hydrophobicity. This property is pivotal for inhibiting the migration of water molecules to the active interface. Specific surface area and pore size distribution analyses (Figure S4) indicated that Ag-TiO₂ and Ag-TiO₂@SiO₂ possess comparable specific surface areas. However, notable differences were observed in their pore size distributions. Ag-TiO₂ exhibited a broad distribution of micropores, mesopores, and macropores. In contrast, Ag-TiO₂@SiO₂ showed a relatively narrower distribution, primarily centered on micropores and small mesopores with a pronounced peak at 3.6 nm, which is characteristic of the mesopores within the SiO₂ shell. This tailored porosity is expected to facilitate the diffusion of CO₂ gas while imposing mass transfer resistance for water molecules. The isothermal water adsorption curves (Figure 2d) strongly support this inference that Ag-TiO₂@SiO₂ exhibited inferior water adsorption capacity, especially in the high relative pressure region, compared to Ag-TiO₂. This can be directly attributed to its hydrophobic surface and mesoporous-dominated structure, which collectively suppress water accumulation on the catalyst surface.

Based on the structural characterization, the photocatalytic CO₂ reduction performance of the as-prepared samples was systematically evaluated in aqueous medium without any sacrificial agent. The reactions were carried out under irradiation from a 300 W xenon lamp, and the gas products were quantified using gas chromatography (GC). As shown in Figure 3a, no reaction products were detected for the exposed SiO₂ nanoparticles (Figure S5), owing to their inherent insulating properties, the unmodified Ag-TiO₂ exhibited strong hydrogen evolution activity with only 5.9% selectivity toward CO, while producing minor amounts of CH₄ and C₂H₄, consistent with its hydrophilic surface property that favors water adsorption and proton reduction. In contrast, after encapsulation

with a porous SiO₂ shell, Ag-TiO₂@SiO₂ achieved 100% selectivity for CO, with H₂ evolution being completely suppressed. The hydrophobic micropores within the CTAB-templated SiO₂ shell create a locally hydrogen-deficient environment, which significantly lowers the surface concentration of reactive H species. As a result, the CO* intermediate formed on the Ag-TiO₂ surface is also prevented from undergoing further hydrogenation to CH₄ or C-C coupling to C₂H₄, and instead desorbs as CO. Although the CO evolution rate over Ag-TiO₂@SiO₂ (6.20 μmol·g⁻¹·h⁻¹) did not increase significantly compared to that of Ag-TiO₂. To decouple the mechanistic contributions of the SiO₂ shell from residual CTAB, we synthesized two reference materials: Ag-TiO₂@D-SiO₂ (CTAB-free with a dense SiO₂ shell) and Ag-TiO₂-CTAB (SiO₂-free with only surface-adsorbed CTAB). Performance testing revealed that while Ag-TiO₂-CTAB, lacking the SiO₂ shell, achieved 53.6% CO selectivity, this remained substantially lower than Ag-TiO₂@SiO₂. Conversely, Ag-TiO₂@D-SiO₂ without CTAB exhibited 100% CO selectivity but demonstrated a markedly reduced CO desorption rate (3.00 μmol·g⁻¹·h⁻¹), primarily due to a significant decrease in specific surface area. To further confirm the origin of hydrophobicity, we removed the SiO₂ shell by NaOH etching. After etching, the CO selectivity of the catalyst dropped to 23% (Figure S6), providing additional evidence that the SiO₂ shell is crucial for inhibiting HER. These findings confirm that the SiO₂ shell serves as the primary barrier against HER, the core function of the porous SiO₂ shell is not to enhance intrinsic activity, but rather to precisely inhibit the hydrocracking pathway by constructing a hydrophobic interfacial microenvironment. This strategic regulation directs the reaction towards near-perfect carbon dioxide reduction selectivity. On the other hand, the SiO₂ shell thickness is another critical parameter influencing catalytic performance. By varying the amount of TEOS added during synthesis, we prepared Ag-TiO₂@SiO₂ samples with different shell thicknesses. Performance evaluation revealed that an excessively thin shell still allows water molecules to reach the reaction interface, resulting in lower CO selectivity. Conversely, an overly thick SiO₂ shell reduces the proportion of active catalytic components in the material, thereby diminishing overall photocatalytic activity. Therefore, rational control of the SiO₂ shell thickness is essential (Figure S7). Inductively coupled plasma (ICP) analysis conducted before and after the 4-h photocatalytic reaction revealed negligible Ag leaching, with a quantified Ag loss of only ~0.16 wt%, thereby confirming the excellent structural stability and retention capability of Ag species in the catalyst under operational conditions (Table S3). The cycling test (Figure 3c) further demonstrated the excellent photocatalytic stability of Ag-TiO₂@SiO₂ over five consecutive runs, confirming the robustness of the core-shell structure [30]. Control experiments (Figure 3d) verified that no CO was detected in the absence of CO₂, light irradiation, or photocatalyst, indicating that the reaction is truly photocatalytic and dependent on all three components. Moreover, isotope labeling experiments using ¹³CO₂ (Figure 3e) clearly demonstrated that the produced CO originated from the supplied CO₂, ruling out contributions from carbonaceous impurities [31].

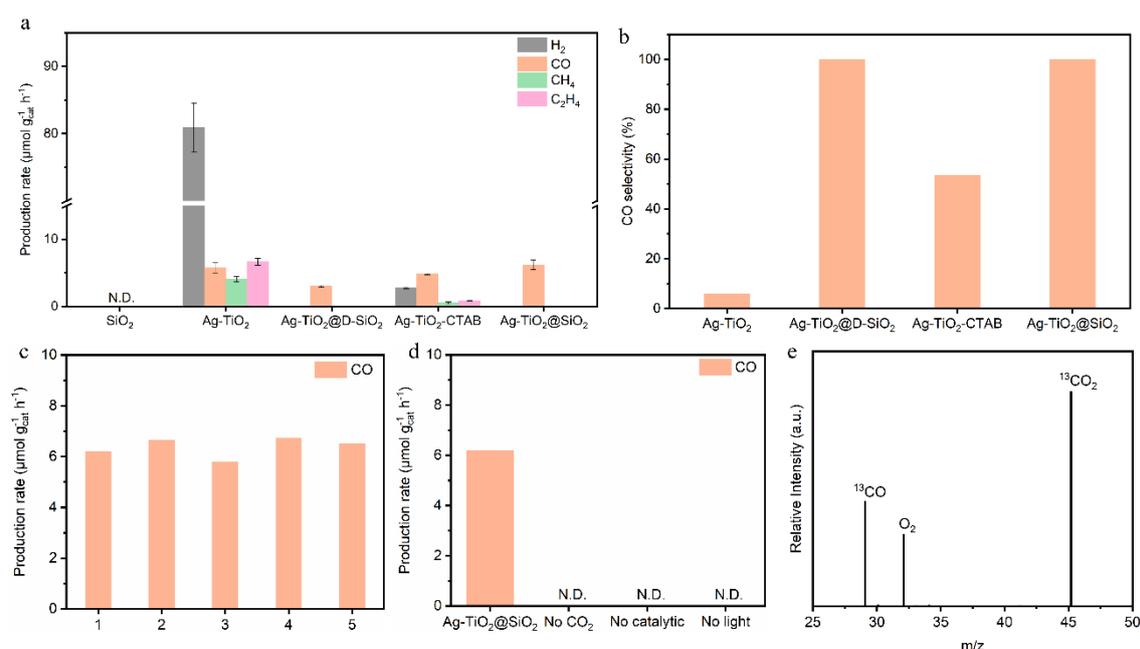


Figure 3. (a) The photocatalytic activity of CO₂ reduction. (b) CO selectivity. (c) Stability tests of CO₂ reduction of Ag-TiO₂@SiO₂. (d) Photocatalytic CO₂ reduction performance under different conditions. (e) CO evolution of the ¹³CO₂ isotope-labeled experiment.

To gain insight into the reaction pathway, in situ diffuse reflectance infrared Fourier transform spectroscopy (DRIFTS) was employed to monitor the intermediate species formed during the CO₂ reduction process [32]. As depicted in Figure 4a, upon irradiation, characteristic peaks emerged at 1706 cm⁻¹ (carbonyl stretch $\nu(\text{C}=\text{O})$ in carboxylic acids), 1550 cm⁻¹ ($\nu_{\text{as}}(\text{OCO})$, the antisymmetric telescopic vibration of OCO), 1409 cm⁻¹ ($\nu_{\text{s}}(\text{COO}^-)$, the symmetrical stretching vibration of COO⁻), and 1253 cm⁻¹ ($\nu(\text{C}-\text{OH})$, the stretching vibration of carboxylic acid hydroxyl group) [22,33]. The presence of these signals confirms that *COOH is a key intermediate in the CO₂ reduction pathway. Additionally, a weak peak at 2160 cm⁻¹ was identified as adsorbed *CO [34]. Coupled with the fact that CO is the major gas product, a plausible reaction pathway can be inferred that CO₂ is activated and hydrogenated to form the *COOH intermediate, which then undergoes dehydration to yield *CO, followed by rapid desorption as gaseous CO. Based on the above results and discussions, a mechanism for the photocatalytic CO₂ reduction over the porous SiO₂-coated Ag-TiO₂ is proposed schematically in Figure 4b. Under light irradiation, TiO₂ generates electron-hole pairs. Given that the work function of Ag (4.26 eV) is higher than that of TiO₂ (4.20 eV), photogenerated electrons in TiO₂ spontaneously transfer to the Ag nanoparticles upon light irradiation, where they participate in reduction reactions. Concurrently, the photogenerated holes remain on TiO₂ and are involved in oxidation reactions, which predominantly occur at oxygen sites [26,35]. The key innovation lies in the porous SiO₂ shell, which constructs a localized hydrophobic microenvironment. The pore channels preferentially allow the diffusion of gaseous CO₂ molecules to the Ag active sites while effectively hindering the access of water molecules. This selective regulation of reactant supply enriches the local concentration of CO₂ around the active sites, thereby drastically suppressing the competition from the HER and ultimately leading to the high selectivity for CO production.

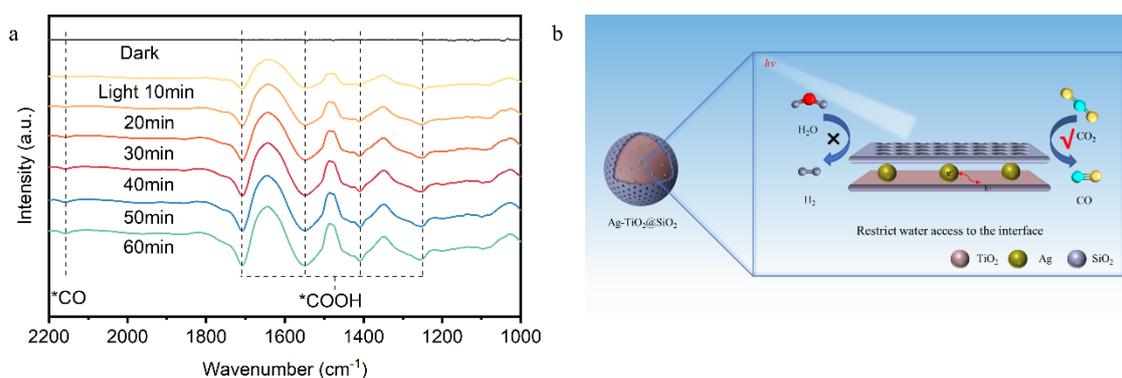


Figure 4. (a) In situ IR spectra of Ag-TiO₂@SiO₂. (b) The mechanism of CO₂ reduction on Ag-TiO₂@SiO₂.

4. Conclusions

In summary, we have developed a porous SiO₂-encapsulated Ag-TiO₂ photocatalyst that achieves 100% selectivity toward CO in the photocatalytic CO₂ reduction reaction without the use of any sacrificial agent. The remarkable enhancement in selectivity is attributed to the core-shell structure, in which the SiO₂ shell acts as a molecular sieve that preferentially permits the diffusion of CO₂ to the active sites while effectively restricting the access of water molecules to the catalytic interface. This work underscores the critical role of interfacial microenvironment engineering in regulating mass transport and suppressing competing reactions in three-phase photocatalytic systems. We believe this SiO₂ encapsulation strategy offers a versatile and scalable pathway for designing highly selective photocatalysts, and it may inspire further exploration of core-shell architectures for efficient solar fuel production and other gas-involved photocatalytic processes.

Supplementary Materials: The following supporting information can be downloaded at: https://media.sciltp.com/articles/others/2602251115362807/MI-25120017-Supplementary_Materials.pdf.

Author Contributions: M.J. conceived and designed the experiments. J.L. performed the catalyst preparation, characterization, and wrote the manuscript. Y.L., contributed to the HRTEM characterizations. Y.W. and Q.G. performed the catalytic tests. Z.G., Y.R., Y.Z., and Q.W. participated in the catalyst preparation and data analysis. The manuscript was written through the contributions of all authors. All authors have read and agreed to the published version of the manuscript.

Funding: This work was supported by the National Natural Science Foundation of China (NSFC, Nos: 52488201, 22171217), National Key R&D Program of China (No. 2024YFF0506100), the Distinguished Young Scholars in Shaanxi Province (No: 2023JC-JQ-12), and the Fundamental Research Funds for the Central Universities.

Data Availability Statement: The authors confirm that the data supporting the findings of this study are available within the article and its supplementary materials.

Conflicts of Interest: The authors declare no conflict of interest.

Use of AI and AI-assisted Technologies: No AI tools were utilized for this paper.

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